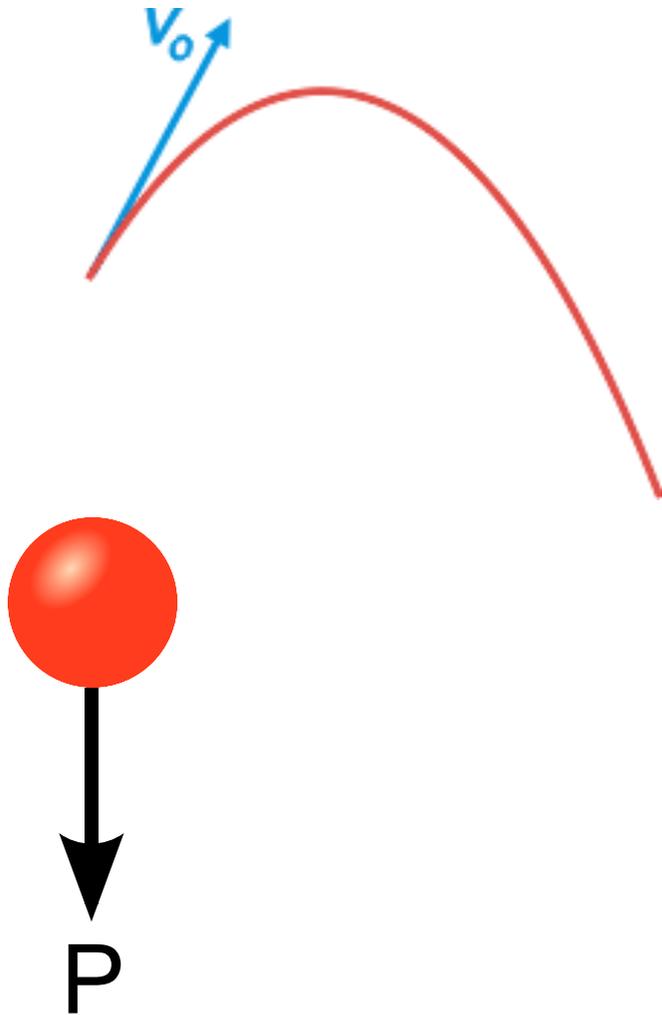


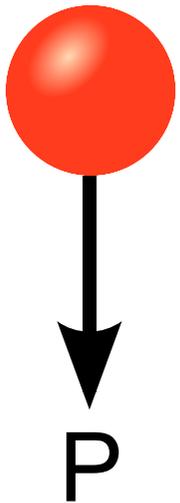
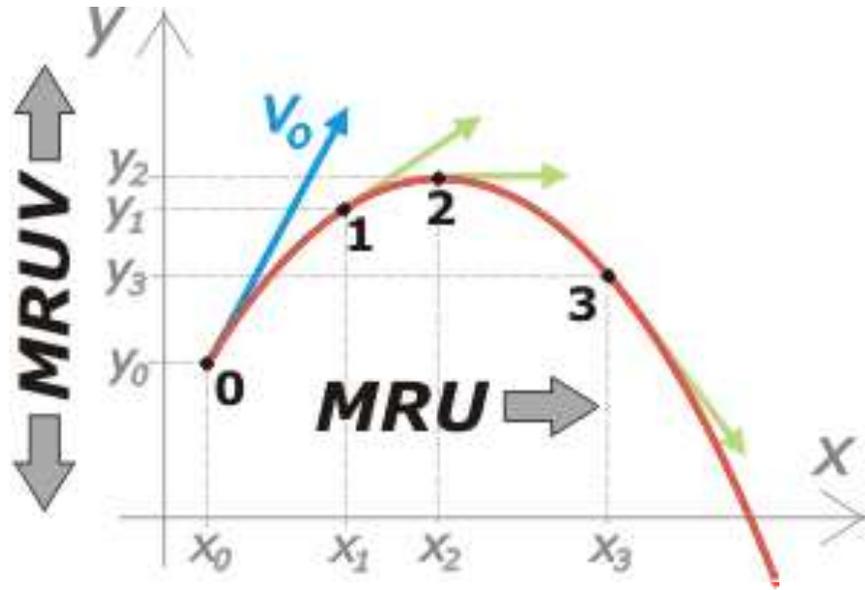
Velocidad límite, viscosidad y modelo de Stokes

<http://materias.df.uba.ar/f1qa2020c1/laboratorios/>

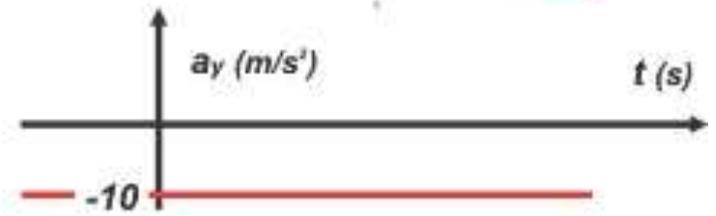
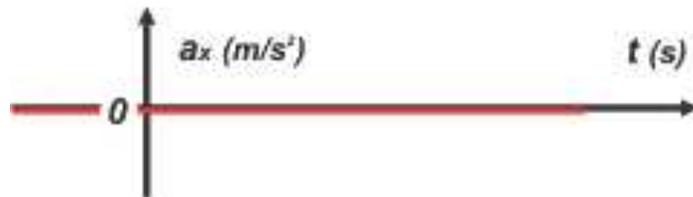
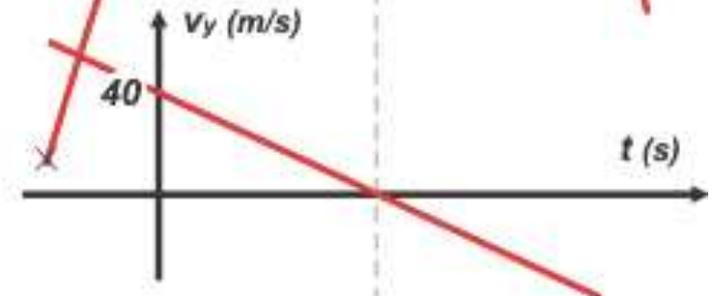
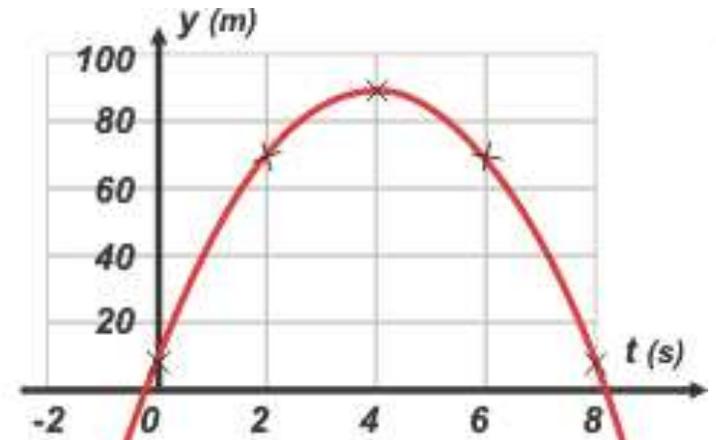
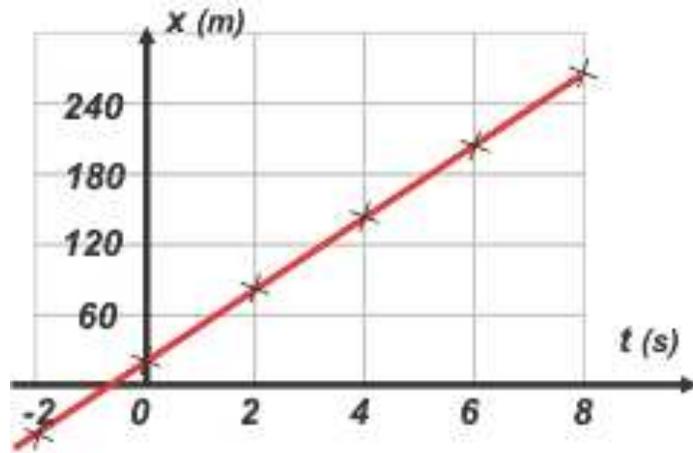
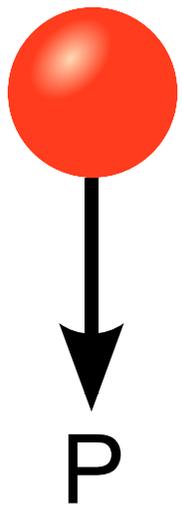
Física 1 (Q): Tiro Oblicuo



Física 1 (Q): Tiro Oblicuo



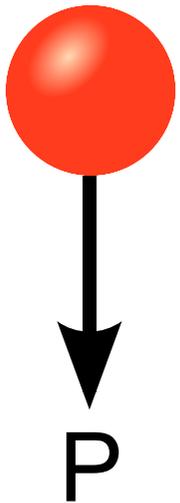
Física 1 (Q): Tiro Oblicuo



Física 1 (Q): Tiro Oblicuo

→ Hipótesis del modelo matemático

- Movimiento en el vacío
- Masa Puntual
- No hay obstáculos



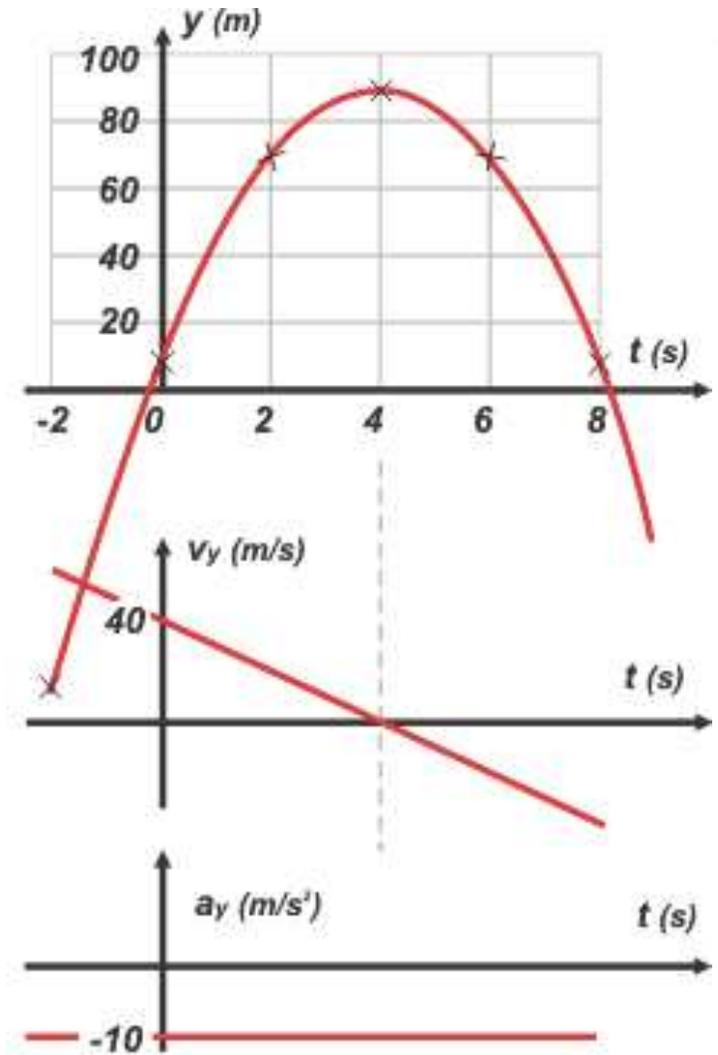
Ecuación de movimiento

$$m \frac{d^2 y}{dt^2} = P$$

Solución

$$y(t) = y_0 + v_0 \cdot t + a \cdot \frac{t^2}{2}$$

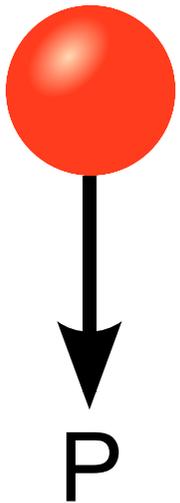
$$\dot{y}(t) = v_y(t) = v_0 + a \cdot t$$



Física 1 (Q): Tiro Oblicuo

→ Hipótesis del modelo matemático

- ~~Movimiento en el vacío~~
- ~~Masa Puntual~~
- No hay obstáculos



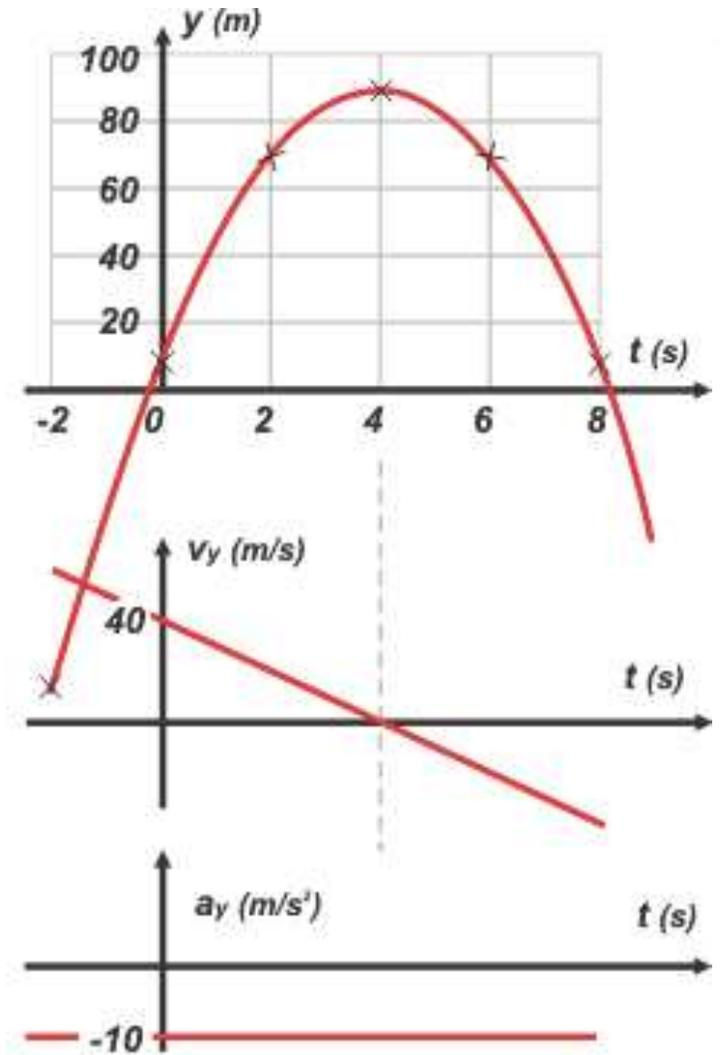
Ecuación de movimiento

$$m \frac{d^2 y}{dt^2} = P$$

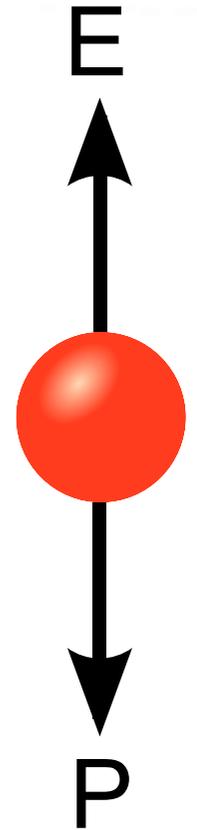
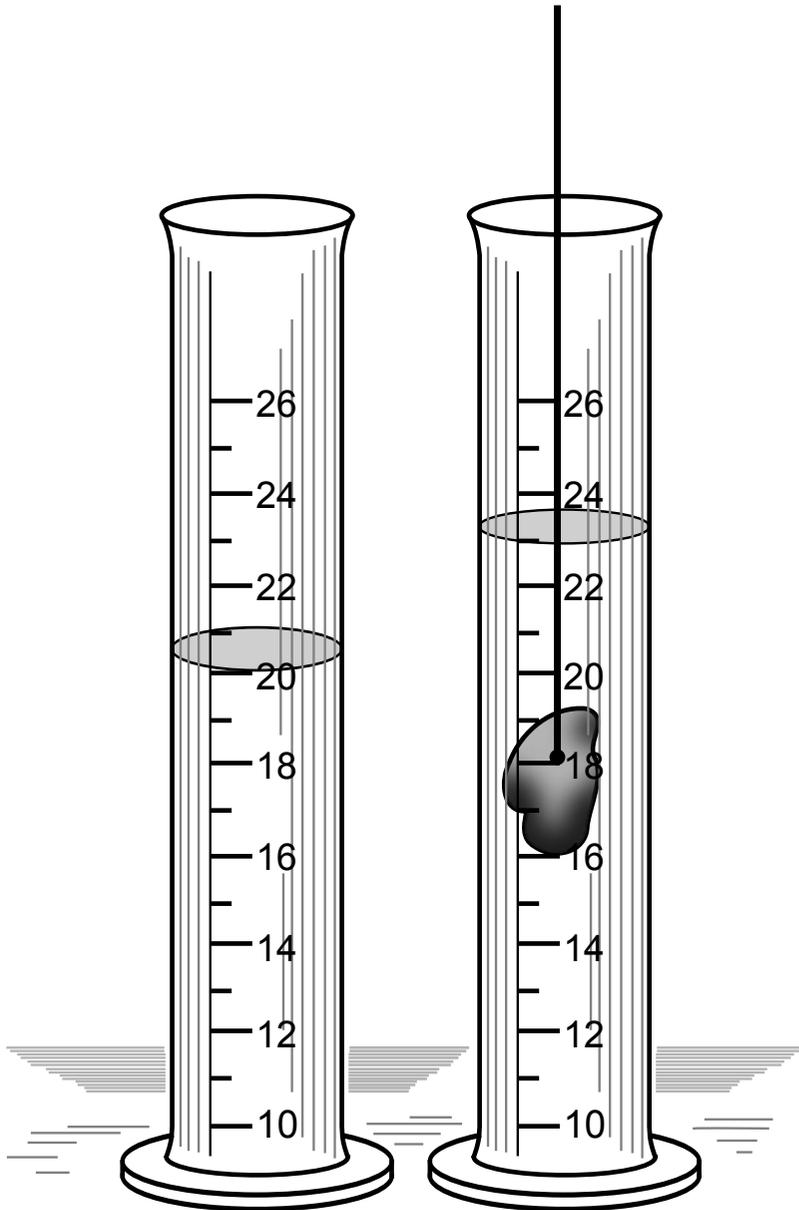
Solución

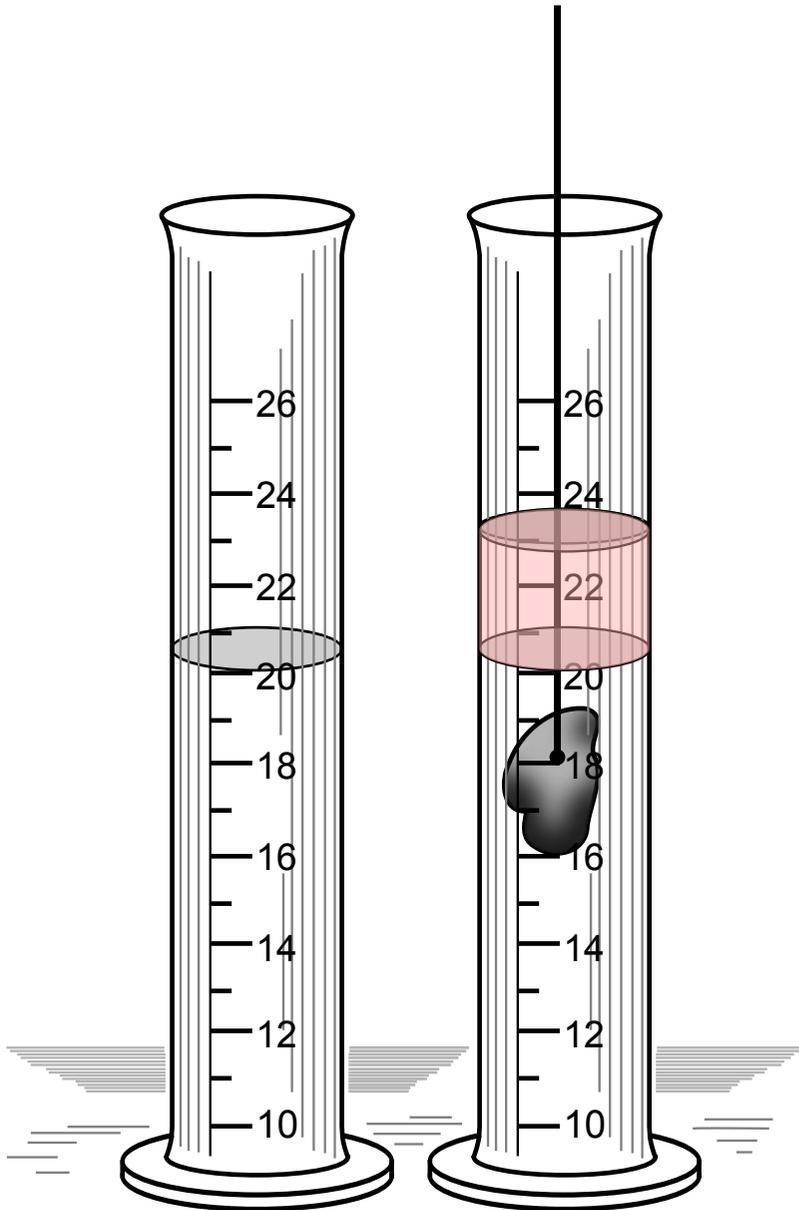
$$y(t) = y_0 + v_0 \cdot t + a \cdot \frac{t^2}{2}$$

$$\dot{y}(t) = v_y(t) = v_0 + a \cdot t$$



Principio de Arquímedes

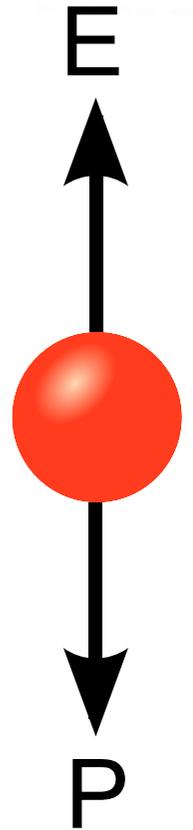


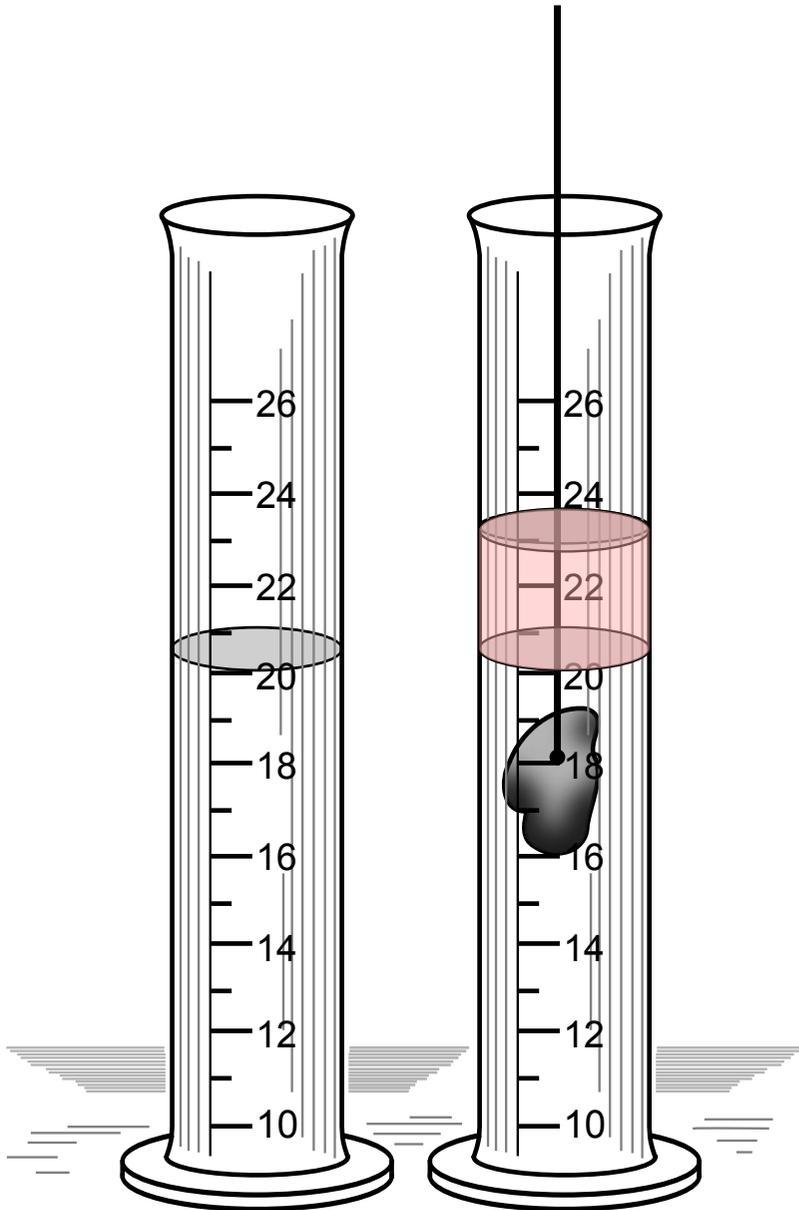


Principio de Arquímedes

Empuje igual al peso del
volumen de líquido
desplazado

Modelo de volumen:
ESFERA





Principio de Arquímedes

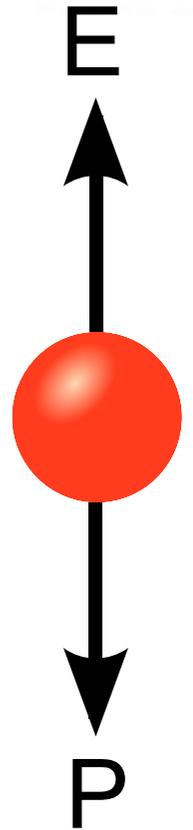
$$E = \frac{4\pi}{3} \cdot r^3 \cdot \rho_L \cdot g$$

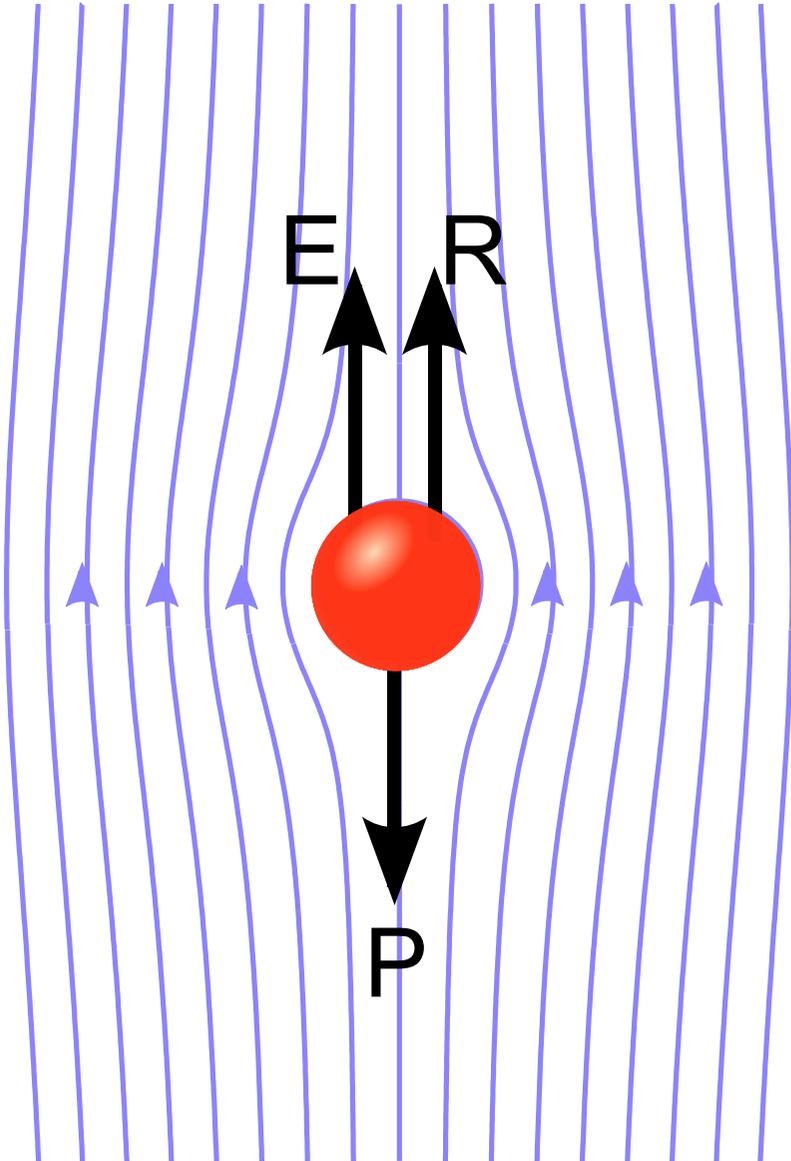
Volumen

Densidad

Ecuación de movimiento

$$m \frac{d^2 y}{dt^2} = P - E$$





Fricción del fluido: Viscosidad

$R = ?$

¿Cómo lo modelamos?

Paréntesis: (Navier-Stokes)

$$\rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{\partial P}{\partial x} + \eta \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x$$

$$\rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) = -\frac{\partial P}{\partial y} + \eta \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right) + \rho g_y$$

$$\rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \eta \left(\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z$$

Paréntesis: (Navier-Stokes)

$$\rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{\partial P}{\partial x} + \eta \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x$$

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$$\rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \eta \left(\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z.$$

Coordenada y

Paréntesis: (Navier-Stokes)

$$\rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{\partial P}{\partial x} + \eta \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x$$

$$\rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) = -\frac{\partial P}{\partial y} + \eta \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right) + \rho g_y$$

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Coordenada y

Terminos convectivos (bajo Re)

Paréntesis: (Navier-Stokes)

$$\rho \left(\frac{\partial v_x}{\partial t} + v_x \frac{\partial v_x}{\partial x} + v_y \frac{\partial v_x}{\partial y} + v_z \frac{\partial v_x}{\partial z} \right) = -\frac{\partial P}{\partial x} + \eta \left(\frac{\partial^2 v_x}{\partial x^2} + \frac{\partial^2 v_x}{\partial y^2} + \frac{\partial^2 v_x}{\partial z^2} \right) + \rho g_x$$

$$\rho \left(\frac{\partial v_y}{\partial t} + v_x \frac{\partial v_y}{\partial x} + v_y \frac{\partial v_y}{\partial y} + v_z \frac{\partial v_y}{\partial z} \right) = -\frac{\partial P}{\partial y} + \eta \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right) + \rho g_y$$

$$\rho \left(\frac{\partial v_z}{\partial t} + v_x \frac{\partial v_z}{\partial x} + v_y \frac{\partial v_z}{\partial y} + v_z \frac{\partial v_z}{\partial z} \right) = -\frac{\partial P}{\partial z} + \eta \left(\frac{\partial^2 v_z}{\partial x^2} + \frac{\partial^2 v_z}{\partial y^2} + \frac{\partial^2 v_z}{\partial z^2} \right) + \rho g_z.$$

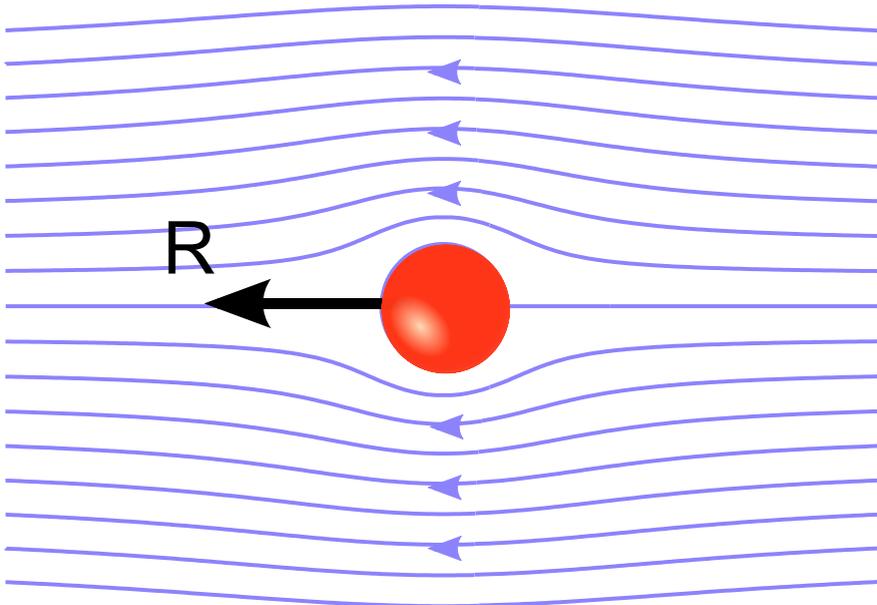
Coordenada y

Terminos convectivos (bajo Re)

Estacionario (velocidad no cambia)

Paréntesis: (Navier-Stokes)

$$0 = -\frac{\partial P}{\partial y} + \eta \left(\frac{\partial^2 v_y}{\partial x^2} + \frac{\partial^2 v_y}{\partial y^2} + \frac{\partial^2 v_y}{\partial z^2} \right)$$



Coordenada y

Terminos convectivos (bajo Re)

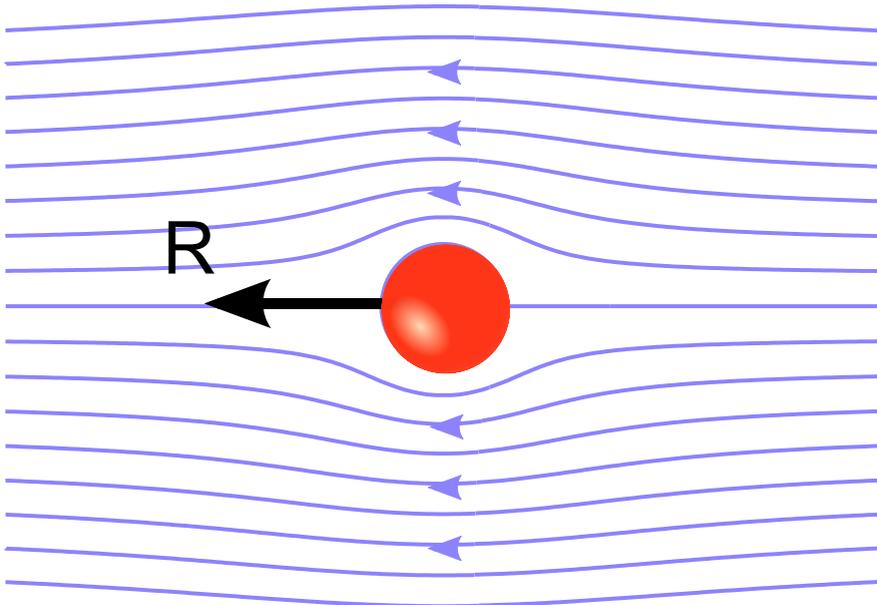
Estacionario (velocidad no cambia)

Objeto esférico en fluido

de extensión infinita

Ley de Stokes

$$R = 6 \cdot \pi \cdot r \cdot \eta \cdot v$$



Coordenada y

Terminos convectivos (bajo Re)

Estacionario (velocidad no cambia)

Objeto esférico en fluido

de extensión infinita

Ley de Stockes y velocidad límite

Ecuación de movimiento

$$m \frac{d^2 y}{dt^2} = P - E - R$$

$$P = m g = \frac{4}{3} \pi \cdot r^3 \cdot \rho_E \cdot g$$

$$E = \frac{4\pi}{3} \cdot r^3 \cdot \rho_L \cdot g$$

$$R = 6 \cdot \pi \cdot r \cdot \eta \cdot v$$

Ley de Stockes y velocidad límite

Ecuación de movimiento

$$m \frac{d^2 y}{dt^2} = P - E - R$$

$$P = m g = \frac{4}{3} \pi \cdot r^3 \cdot \rho_E \cdot g$$

$$E = \frac{4\pi}{3} \cdot r^3 \cdot \rho_L \cdot g$$

$$R = 6 \cdot \pi \cdot r \cdot \eta \cdot v$$

Soluciones

$$m \frac{d^2 y}{dt^2} = P - E - R = 0 \quad \rightarrow \quad v_{lim} = \frac{2}{9} \cdot \frac{r^2 g}{\eta} \cdot (\rho_E - \rho_L)$$

$$m \frac{d^2 y}{dt^2} = P - E - 6 \cdot \pi \cdot r \cdot \eta \cdot \frac{dy}{dt}$$

$$\rightarrow \dot{y}(t) = v_y(t) = v_{lim} (1 - \exp(-\alpha t))$$

Ley de Stockes y velocidad límite

Modelo para trabajar

Terminos convectivos (bajo Re)

Estacionario (velocidad no cambia)

Objeto esférico en fluido de extensión infinita

Velocidad límite:

$$v_{lim} = \frac{2}{9} \cdot \frac{r^2 g}{\eta} \cdot (\rho_E - \rho_L)$$

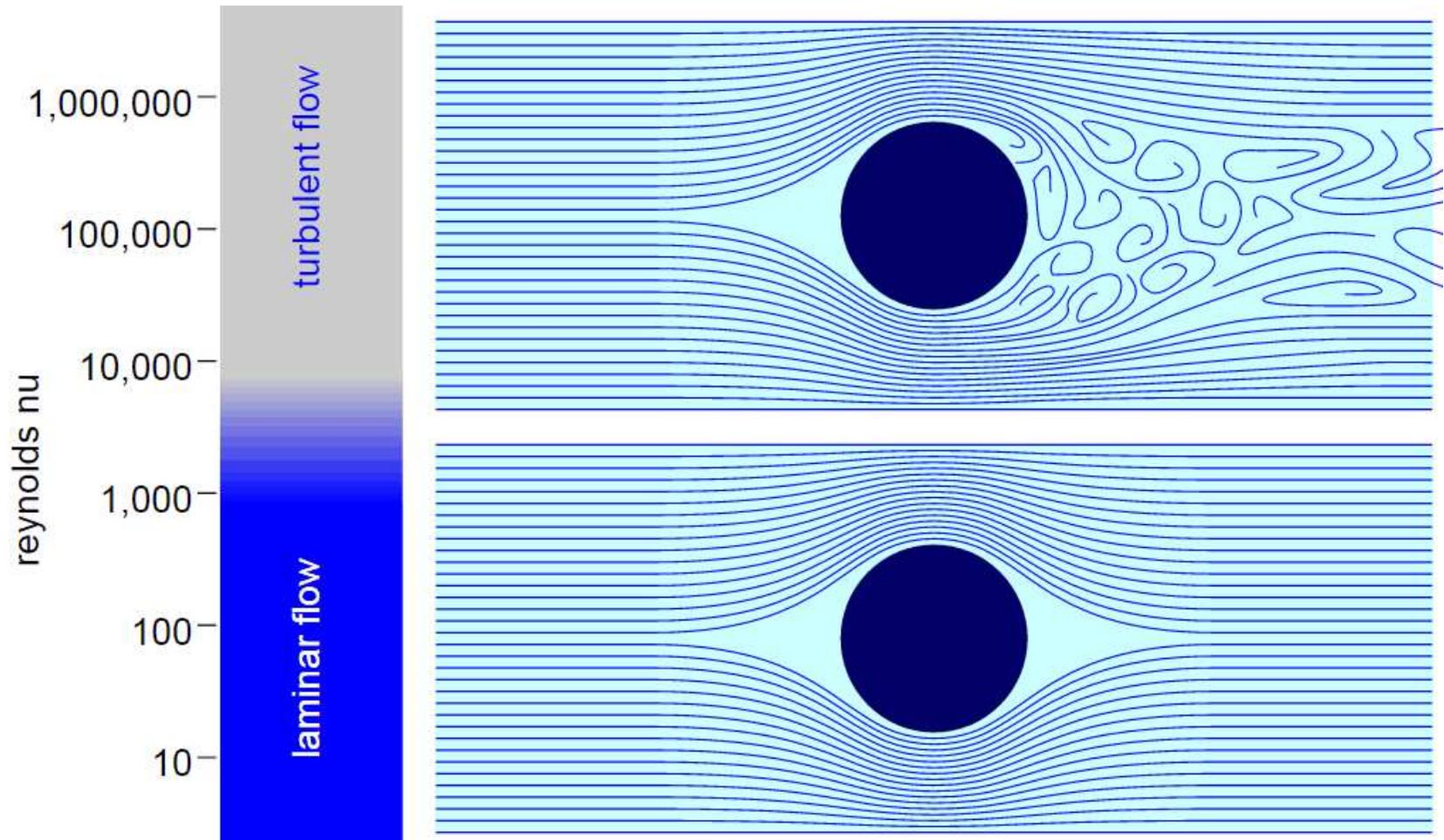
Velocidad en el tiempo:

$$v_y(t) = v_{lim}(1 - \exp(-\alpha t))$$

Aproximaciones: Reynolds

Terminos convectivos (bajo Re)

$$Re = \frac{\rho_L \cdot v_{lim} \cdot d}{\eta}$$

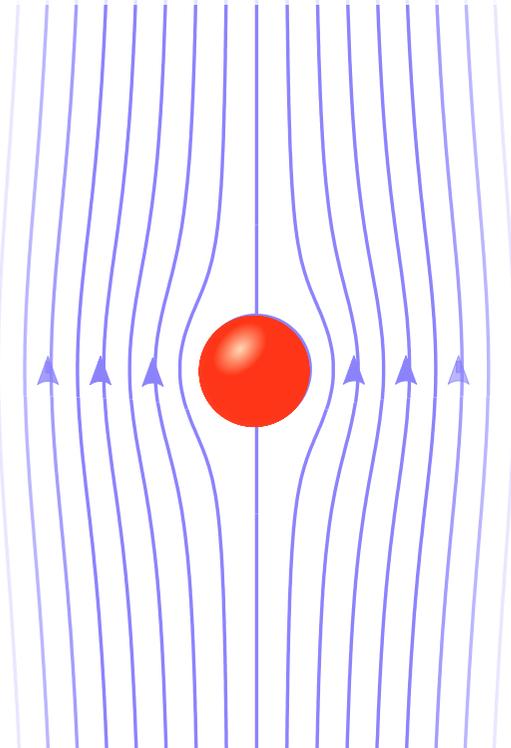


Corrección de Ladenburg

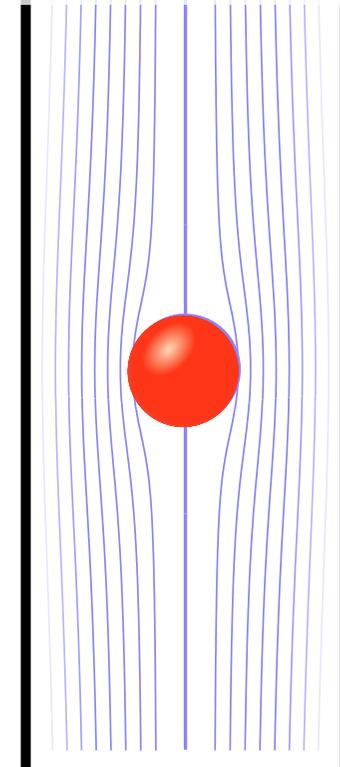
Objeto esférico en fluido de extensión infinita

$$\lambda = 1 + 2.4 \frac{r}{r_{tubo}} \quad \longrightarrow \quad v_{lim} = \lambda \cdot v_{medida}$$

Modelo Stockes



Corrección Ladenburg



Presentación de la actividad

➔ **Cuaderno de laboratorio**

➔ **Dos series de videos**

Caída libre en un fluido

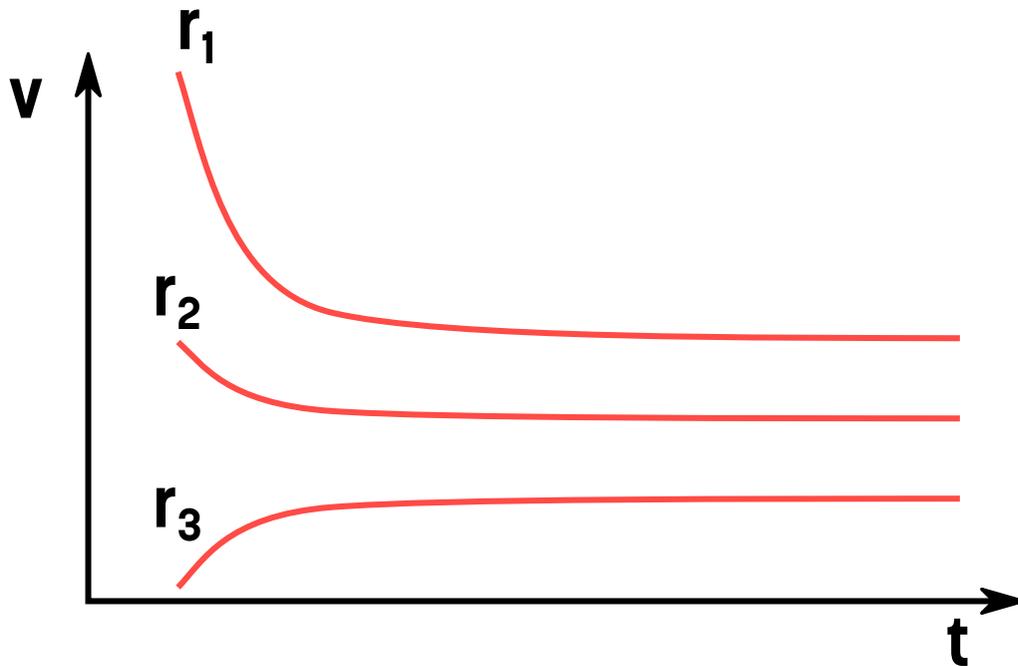
➔ **Papers y datos**

➔ Cuaderno de laboratorio

➔ Dos series de videos

Caída libre en un fluido

➔ Papers y datos



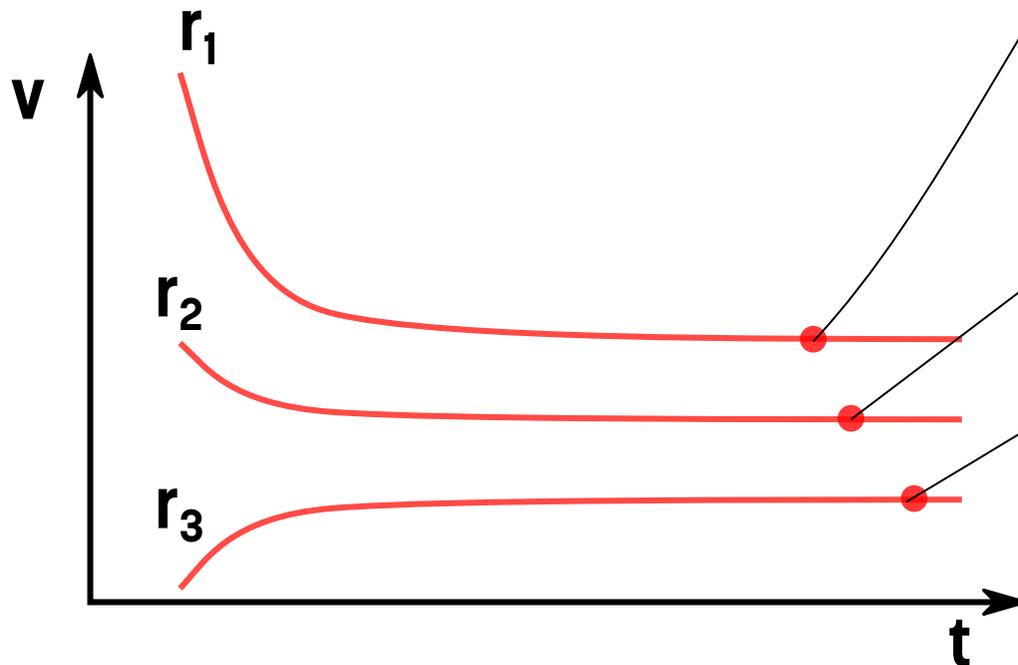
r	v_{final}
r_1	
r_2	
r_3	

➔ Cuaderno de laboratorio

➔ Dos series de videos

Caída libre en un fluido

➔ Papers y datos



r	v_{final}
r_1	
r_2	
r_3	

➔ Cuaderno de laboratorio

➔ Dos series de videos

Caída libre en un fluido

➔ Papers y datos

r	V_{final}
r_1	●
r_2	●
r_3	●

$$\lambda = 1 + 2.4 \frac{r}{r_{\text{tubo}}}$$

$$v_{\text{lim}} = \lambda \cdot v_{\text{medida}}$$

$$v_{\text{lim}} = \frac{2}{9} \cdot \frac{r^2 g}{\eta} \cdot (\rho_E - \rho_L)$$

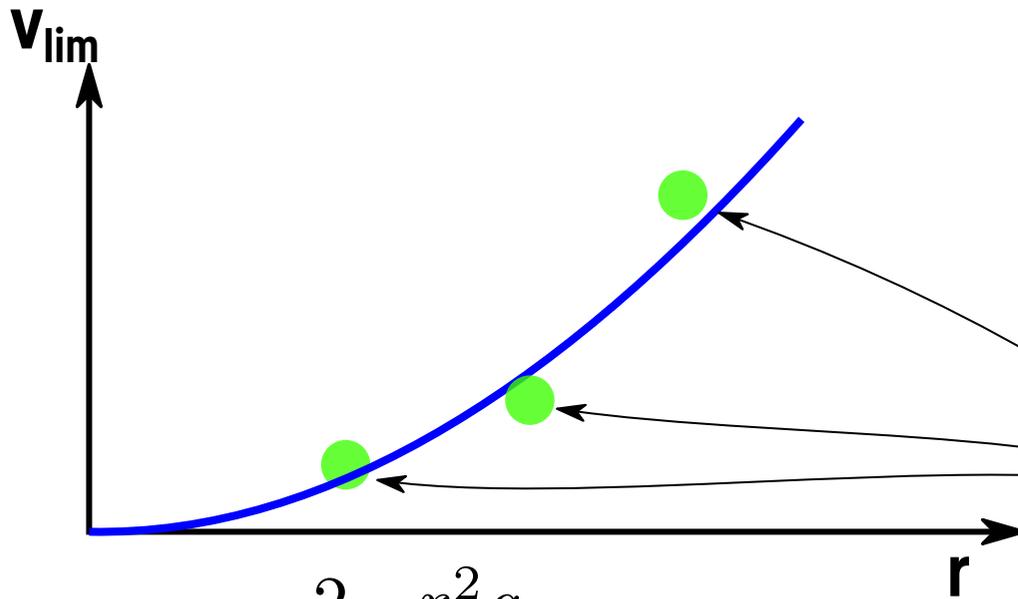
➔ Cuaderno de laboratorio

➔ Dos series de videos

Caída libre en un fluido

➔ Papers y datos

r	V_{final}
r_1	●
r_2	●
r_3	●



$$v_{\text{lim}} = \frac{2}{9} \cdot \frac{r^2 g}{\eta} \cdot (\rho_E - \rho_L)$$

$$\lambda = 1 + 2.4 \frac{r}{r_{\text{tubo}}}$$

$$v_{\text{lim}} = \lambda \cdot v_{\text{medida}}$$

➔ Cuaderno de laboratorio

➔ Dos series de videos

Caída libre en un fluido

➔ Papers y datos

$$v_{lim} = \frac{2}{9} \cdot \frac{r^2 g}{\eta} \cdot (\rho_E - \rho_L)$$